

INSTRUCTIONS FOR

METHANE FROM COMMUNITY WASTE
SYSTEMS ANALYSIS (COWSA) MODEL

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ABBREVIATIONS

BMP	Biochemical Methane Potential
BOD	Biological Oxygen Demand
BVS	Biodegradable Volatile Solids
CMD	Command Mode Indicator (in Lotus 1-2-3)
COD	Chemical Oxygen Demand, a measure of total organics concentration, typically used for characterization of wastewater
COWSA	Community Waste Systems Analysis
CPI	Characters Per Inch
CSTR	Continuously Stirred Tank Reactor
ECH	Equipment Cost Handbook
ECSA	Energy Crop Systems Analysis
gpd	gallons per day
GRI	Gas Research Institute
HHV	Higher Heating Value
HRT	Hydraulic Retention Time
k	First order reaction rate coefficient
kwh	Kilowatt hour
MGD, mgd	Million Gallons per Day
MMBtu	Million British Thermal Units
MMscf	Million standard cubic feet
MSW	Municipal Solid Waste
NMVFR	Non-Mixed Vertical Flow Reactor
O&M	Operation and Maintenance
PDA	Process Development Allowance
Q	Wet Tons Feed Per Day
RDF	Refuse Derived Fuel
RS&H	Reynolds, Smith and Hills, A-E-P, Inc.
scf	Standard Cubic Foot, at 1 atmosphere (14.7 psi) and 0°C (32°F)
SNG	Substitute Natural Gas
SRT	Solids Retention Time
SS	Suspended Solids
STP	Standard Temperature and Pressure

TPD, tpd Tons Per Day
TBtu 10^{12} British Thermal Units
TS Total Solids
TSS Total Suspended Solids
VS Volatile Solids, or combustible solids
VSS Volatile Suspended Solids
VSCE Volatile Solids Conversion Efficiency
v/v/d volume methane/unit reactor volume/day
VSLR Volatile Solids Loading Rate (E.g.: lbs VS added/cu ft reactor
volume/day, or grams VS/liter reactor volume/day
VDS Volatile Dissolved Solids

INTRODUCTION

The Methane from Community Waste Systems Analysis (COWSA) model was developed using Lotus 1-2-3® Release 2 software. A basic knowledge of this software is required, and will allow the user to easily interact with the COWSA model. Macros have been integrated into the COWSA model to make it menu driven and relatively "user friendly". The user should also be familiar with the systems and terminology used for a community waste biogasification facility.

COWSATF1 is the first version of the COWSA model that calculates a tipping fee (\$/ton MSW), whereby gas price is an input. There exists a parallel version (COWSAGC1) that calculates gas price; using tipping fee as an input.

The COWSA spreadsheet consists of seven sections arranged as shown in Figure 1, Community Waste Systems Analysis Model-Spreadsheet Map. These sections contain input and output areas, calculation and process flowsheet areas, and an area for the spreadsheet macros.

STARTING COWSA

Start the Lotus 1-2-3, Release 2 program using DOS Version 2.0, 2.1, 3.0, or 3.1 on an IBM PC, XT, AT® or compatible computer. When 1-2-3 is in the ready mode, type / File Retrieve (or /FR) COWSATF1 or COWSAGC1 and hit the ENTER (RETURN) key. File retrieval takes between 10 and 70 seconds, depending on the computer. When the file is retrieved, the initial screen as shown in Figure 2 should appear on the monitor.

MENU COMMANDS AND OPTIONS

The second line from the top of the initial screen contains the main menu commands. The COWSA model starts under macro control (as noted by the CMD indicator at the bottom of the screen) each time the file is initiated. As in 1-2-3, the COWSA menu commands can be selected by two methods.

A5	I5 INPUT/OUTPUT Input Output Section Section H38	T1 INPUT/OUTPUT Technical Assumptions AD25	AF1 CONVERSION High Moisture Feeds BL38	BN25 RESIDUE PROCESSING Thermal Only (Option II, Boiler)	CW1 COST / FINANCIAL & INPUT/OUTPUT Cost (Module) Assumptions DM55
A41	FRONT END (Refuse Separation RDF Module R76	T27 FRONT END Feed Input: Wet (High Moisture)	AF40 CONVERSION Low Moisture Feeds BL80	BN56 RESIDUE PROCESSING Thermal Only (Option III, Power Plant)	CU54 COST / FINANCIAL Assumptions CW61 Cost Table CU100
A79	FRONT END Sewage Treatment Module R189	AD91 CONVERSION (Low Moisture Feeds) Wet Oxidation Option BL151	AD82 CONVERSION Dry (Low Moisture)	CU100 For Future Use RESIDUE PROCESSING Gasification & Composting AV154 CONVERSION (Intermediate) Gas Clean-up BL185	CS121 C/F Credit Tbl DM137 CW139 COST / FINANCIAL & INPUT/OUTPUT Levelized Cost Input & Financial Assumptions DM223 CW225 COST/ FINANCIAL Levelized Cost Summary DM228
A191	MACRO SECTION	AD189 ENERGY Process Energy Module BL250	AD250		

FIGURE 1 Community Waste Systems Analysis
(COWSA) Model - Spreadsheet Map

MENU

A1: PR 'METHANE FROM COMMUNITY WASTE SYSTEMS ANALYSIS (COWSA)

INPUT TRAVEL PRINT QUIT

Enter inputs into various sections of the model

A B C D E F G H

1 METHANE FROM COMMUNITY WASTE SYSTEMS ANALYSIS (COWSA)

2 FILENAME: COWSTFL3

3 DATE: 16 JUNE 88

4

5 INPUT SECTION

6

7 MGD sewage

8 Tons per day MSW (7 days/wk)

9 % Total Solids MSW

10 % Volatile Solids (of TG) MSW

11 % Biodegradable Volatile Solids (of VS) MSW

12 SNG sales price

13 Solid residue processing option:

14 1 = Landfill

15 2 = Incinerate - recover process heat

16 3 = Power plant - recover process heat & generate power

17 4 = Wet Oxidation

18 Low, average or high cost estimate (L, A, H)

19 Base year dollars (1980 - 1990)

20 A 1987

21 HIGH MOISTURE LOW MOISTURE

22 CMD

23 27-Jun-88 02:18 PM

FIGURE 2. Initial Screen Display for COWSA

First, move the cursor using the right arrow and left arrow keys to highlight the desired command, then hit the ENTER key. The second method is to type the first letter of the desired command. If there are two or more menu commands that begin with the same letter, the second method will select the first command (from left-to-right in the menu) that begins with that letter.

During operation of the model, there are occasions when the user will be working out of macro control (the CMD indicator will be off). To return to macro control and call up the main menu hold down the Alt key and type M.

There are also menu options to be selected from within the main menu commands. These options as shown in Figure 3, can be selected by the same methods as previously described for menu commands. When viewing the Input, Travel, and Print Options menus, the user can use the Esc key to recall the main menu. The Commands available from the main menu are INPUT, TRAVEL, PRINT and QUIT.

INPUT Command: The INPUT command allows the user to enter or change input data into the various sections of the COWSA model. After the INPUT command has been selected, the INPUT Options menu is displayed. Figure 4 shows the INPUT Options and the selections available with these options. The five options available within the Input command are PRIMARY, SEWAGE TREATMENT, ASSUMPTIONS, COST/CREDIT, and FINANCIAL.

PRIMARY: This option, when selected, allows the user to enter or modify input data within the Primary Input Section. A sample Primary Input Section screen is shown by Figure 5.

SEWAGE TREATMENT: This input option allows the user to enter or modify input data to the Sludge/Water Hyacinth Module (adapted from Black & Veatch). This module contains three steps; Primary Treatment, Hyacinth Ponds, and Hyacinth Productivity. Step 2, Hyacinth Ponds, contains four options for determining effluent BOD & SS, retention time, loading rate, and surface area of ponds (in acres). Select the option that is a known parameter, enter the required values, and the spreadsheet will calculate the other three quantities.

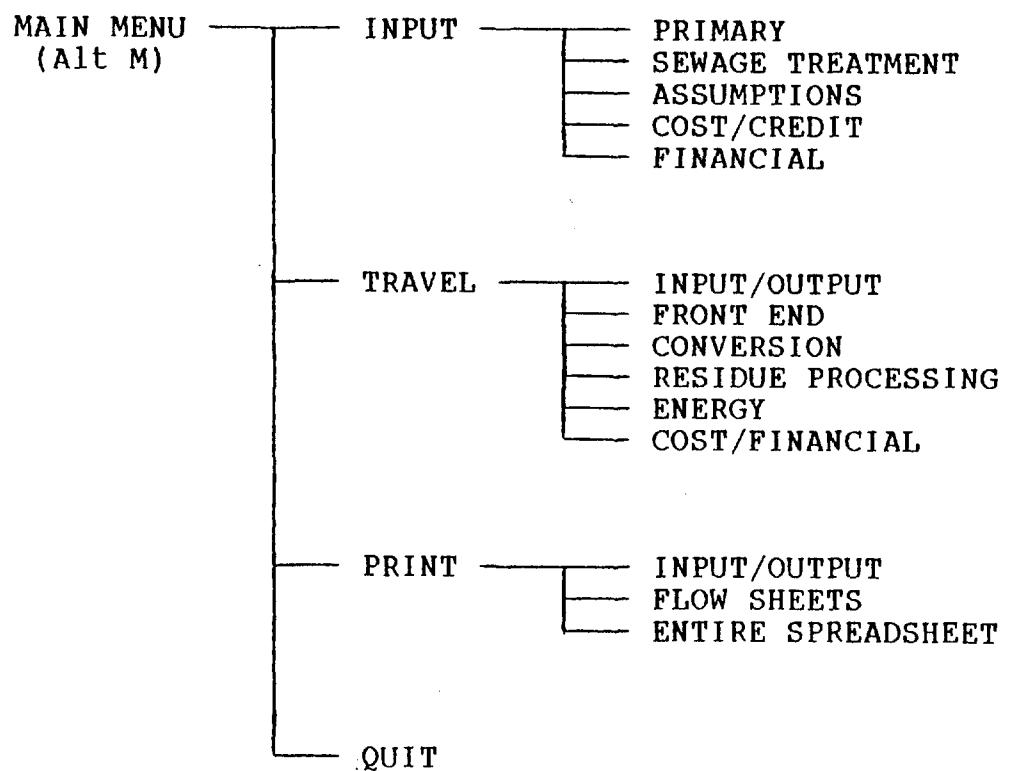


Figure 3. Main Menu Commands

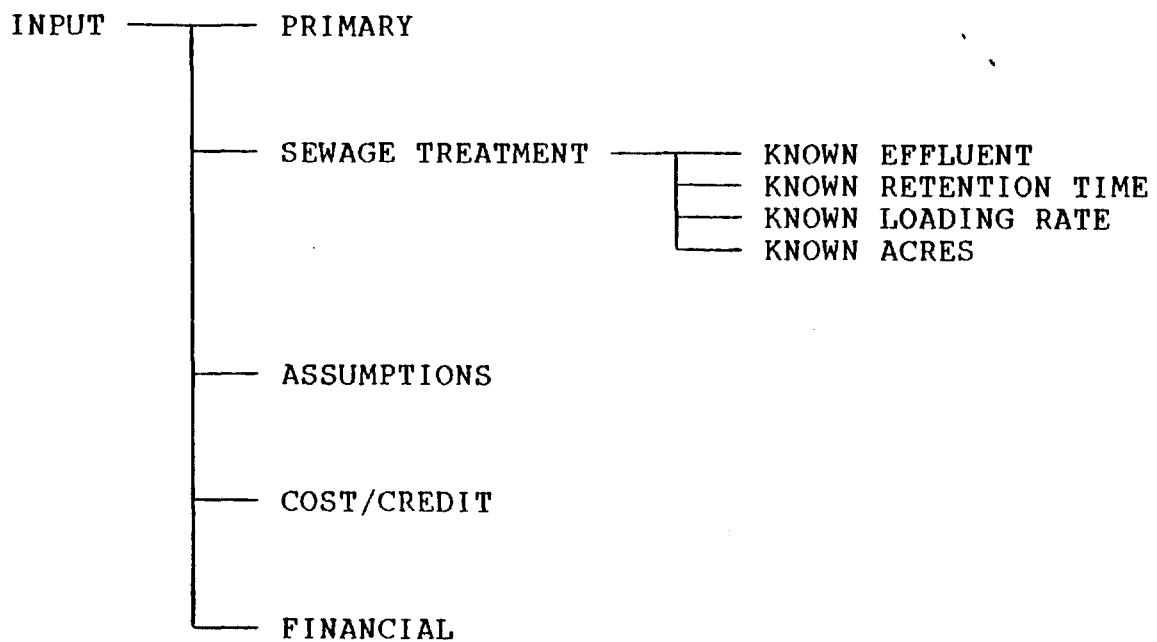


Figure 4. Input Command Options Flowchart

READY

G24: U [W7] 140
Are all entries correct? (Y/N)

5	A	B	C	D	E	F	G	H
6				INPUT SECTION				
7	MGD sewage				20	MGD		
8	Tons per day MSW (7 days/wk)				600	tpd		
9	% Total Solids MSW				74.0	%		
10	% Volatile Solids (of TS) MSW				73.0	%		
11	% Biodegradable Volatile Solids (of VS) MSW				87.0	%		
12	SNG sales price				\$3.00	/MMBtu		
13	Solid residue processing option:				3			
14	1 = Landfill							
15	2 = Incinerate - recover process heat							
16	3 = Power plant - recover process heat & generate power							
17	4 = Wet Oxidation							
18	Low, average or high cost estimate (L, A, H)							
19	Base year dollars (1980 - 1990)							
20	SRT							
21	SRT/HRT ratio							
22	% CH4 in biogas (both 55% or 85%)				2.00	1.00		
23	Digester temperature				55	55	%	
24					95	140	deg F	
	27-Jun-88 02:15 PM				CMD			

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FIGURE 5. Primary Input Section Screen Display

ASSUMPTIONS: This option allows the user to modify the technical assumptions used in the COWSA model.

COST/CREDIT: This option allows the user to modify the cost and credit data within the Cost Module. The Cost Module contains the following seven categories: Refuse Separation, Sewage Treatment, Conversion, Gas Cleanup/Compression, Solid Residue Processing, Compostable Residue Processing, and Other.

FINANCIAL: This option allows the user to modify the financial assumptions used in the Levelized Cost Module.

When the desired input option has been selected, the macro will move the cursor to the corresponding input locations. Key in the desired value and then hit ENTER for each of the required input items. If the pre-existing value is acceptable, just hit ENTER to proceed to the next input item. Do not use the arrow keys to move the cursor during the input procedure, use only the ENTER key. If your system is too slow between entries, set it for manual recalculation by typing /WGRM.

After entering the final required value in any of the input options, the macro will prompt the user with "Are all entries correct? (Y/N)". If not, type N and hit ENTER to go through the input procedure again. If the values are all correct, type Y, and hit ENTER (or just hit ENTER) and the macro will advance to the Output Section. Press ENTER again and the Levelized Cost and Net Total Levelized Tipping Fee will be displayed as shown in Figure 6, and control is returned to the main menu.

TRAVEL Command: The TRAVEL command permits the user to move to, view and explore the various sections of the COWSA spreadsheet. When the TRAVEL command is selected, the TRAVEL Options Menu is displayed. There are six options available in the TRAVEL Options Menu that correspond to the six main sections of the spreadsheet. Refer to Figure 1, COWSA Model Spreadsheet Map. These options (sections) are INPUT/OUTPUT, FRONT END, CONVERSION, RESIDUE PROCESSING, ENERGY, AND COST/FINANCIAL.

MENU

I32: PR 'NET TOTAL
INPUT TRAVEL PRINT QUIT
Enter inputs into various sections of the model

	I	J	K	L	M	N	O	P
13	vol. methane/vol. reactor/day					1.78	2.10	v/v/d
14	Volatile Solids Loading Rate (VSLR)				0.44	0.43	1b VS/cf-day	
15	% of gross methane production				5.2	94.8	%	
16								
17	LEVELIZED COST				1987 \$/ton		% of Total Cost	
18	Refuse Separation				\$11.7735		23.58%	
19	Sewage Treatment				\$6.5961		13.21%	
20	Conversion - High Moisture				\$1.1034		2.21%	
21	Conversion - Low Moisture				\$7.3068		14.63%	
22	Gas Cleanup				\$2.1649		4.34%	
23	Solid Residue Processing				\$20.9897		42.03%	
24	TOTAL COST				\$49.9343		100.00%	
25								
26								
27	Gas Credit				(\$13.2366)			
28	Sewage Credit				(\$6.6667)			
29	Byproduct Credit				(\$4.6823)			
30	TOTAL CREDIT				(\$24.5856)			
31								
32	NET TOTAL				\$25.3487			
27-Jun-88 02:16 PM	CMD							

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FIGURE 6. Sample Output Section Screen Display

When one of the TRAVEL options (except ENERGY) is selected, the user will have a choice of destinations within that section. Figure 7, Travel Command, Options Flowchart shows the six TRAVEL options and the choice of destinations for each option. The ENERGY option has only one destination and therefore no additional selection is needed for "travel" to the Process Energy Module.

Once a TRAVEL option and destination have been selected, the cursor advances to the chosen destination. The spreadsheet is no longer under macro control. The user is now free to move around the spreadsheet using the arrow keys, page down, page up, tab, shift tab, and the goto (F5) key with a range name or cell address.

To recall the main menu and return to macro control, hold down the Alt key and type M.

PRINT Command: The PRINT command initiates macros to format and print various sections of the spreadsheet, or the entire spreadsheet. When the PRINT command is selected, the PRINT Options Menu is displayed. The available PRINT options are INPUT/OUTPUT, FLOW SHEETS, and ENTIRE SPREADSHEET. The PRINT Options and the selections available with them are presented in Figure 8. Examples of the INPUT/OUTPUT and FLOW SHEETS printouts are displayed in Figures 9 through 16.

INPUT/OUTPUT: Prints the primary Input Section and Output Section, 10 characters per inch (CPI), on 8½" x 11" paper.

!
FLOW SHEETS: Prints process flowsheets for the RDF Module, Conversion Module, Gas Clean-up Module and Residue Processing Module. The following list gives the minimum paper size (width x height) and specifies the CPI value for each Flow Sheet Option.

RDF Module	:	11"x 8½", 17 CPI
Conversion Module		
- High Moisture Feeds	:	11"x 8½", 17 CPI
- Low Moisture Feeds	:	11"x 8½", 17 CPI
- Wet Oxidation Option	:	14"x 11", 17 CPI
Gas Clean-up Module	:	11"x 8½", 17 CPI
Residue Processing Module		
- Thermal Only (Option II)	:	11"x 8½", 17 CPI
- Thermal & Power (Option III):		14"x 8½", 17 CPI

ENTIRE SPREADSHEET: Prints the entire COWSA spreadsheet, 17 CPI, on 25 sheets of 14" x 11" paper.

QUIT Command: This command macro removes the main menu, ends macro control of the spreadsheet, and returns the computer to the 1-2-3 READY mode. These same functions can be accomplished by pressing the Escape key when the main menu is displayed. The CMD indicator will be OFF. This allows the user to end the COWSA session or to move throughout the spreadsheet using the arrow, page down, page, tab, shift tab, and goto (F5) keys. To recall the main menu and return to macro control, hold down the Alt key and type M.

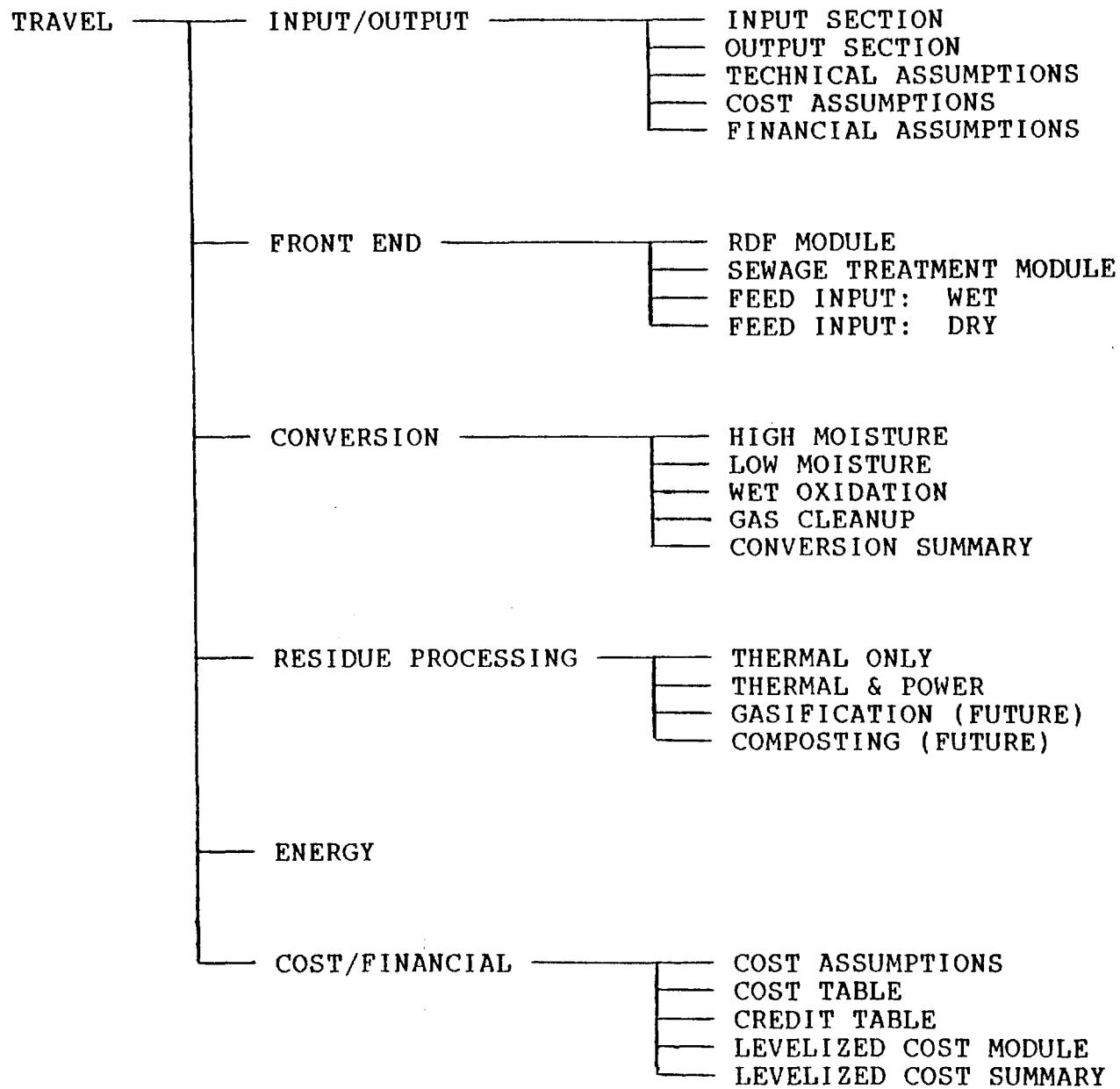


Figure 7. Travel Command Options Flowchart

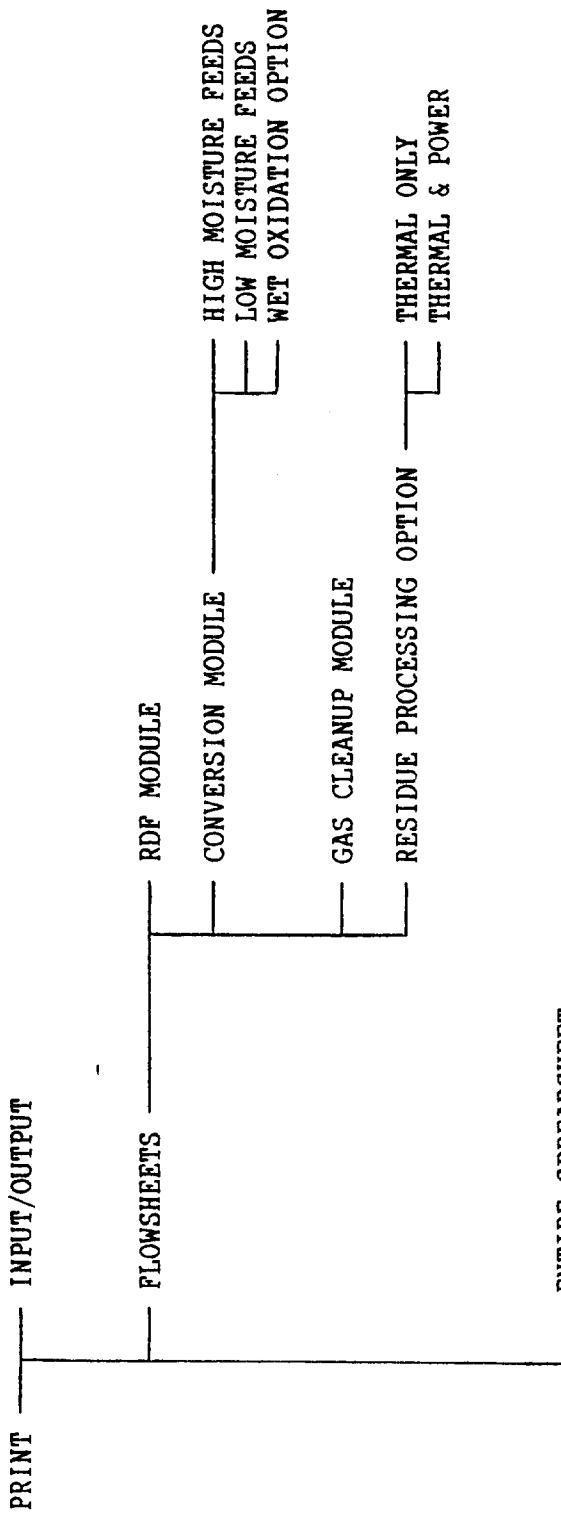


Figure 8. Print Command Options Flowchart

FIGURE 9. Input/Output, Print Example

INPUT SECTION

MGD sewage	20 MGD
Tons per day MSW (7 days/wk)	600 tpd
% Total Solids MSW	74.0 %
% Volatile Solids (of TS) MSW	73.0 %
% Biodegradable Volatile Solids (of VS) MSW	87.0 %
SNG sales price	\$3.00 /MMBtu
Solid residue processing option:	3
1 = Landfill	
2 = Incinerate - recover process heat	
3 = Power plant - recover process heat & generate power	
4 = Wet Oxidation	
Low, average or high cost estimate (L, A, H)	A
Base year dollars (1980 - 1990)	1987
	HIGH MOISTURE LOW MOISTURE
SRT	10.00 20.00 days
SRT/HRT ratio	2.00 1.00
% CH ₄ in biogas (both 55% or 85%)	55 55 %
Digester temperature	95 140 deg F

OUTPUT SECTION

Net methane production per day	2.79 MMscf/day
Net energy production per year	0.97 10E12 Btu/yr
Pond area	163.5 acres
	HIGH LOW MOISTURE
Volatile Solids Conversion Efficiency %	54.26 69.48 %
Gross methane yield	4.08 4.87 scf CH ₄ /lb VSa
vol. methane/vol. reactor/day	1.78 2.10 v/v/d
Volatile Solids Loading Rate (VSLR)	0.44 0.43 lb VS/cf-day
% of gross methane production	5.2 94.8 %

LEVELIZED COST	1987 \$/ton	% of Total Cost
Refuse Separation	\$11.7735	23.58%
Sewage Treatment	\$6.5961	13.21%
Conversion - High Moisture	\$1.1034	2.21%
Conversion - Low Moisture	\$7.3068	14.63%
Gas Cleanup	\$2.1649	4.34%
Solid Residue Processing	\$20.9897	42.03%
TOTAL COST	\$49.9343	100.00%
 Gas Credit	(\$13.2366)	
Sewage Credit	(\$6.6667)	
Byproduct Credit	(\$4.6823)	
TOTAL CREDIT	(\$24.5856)	

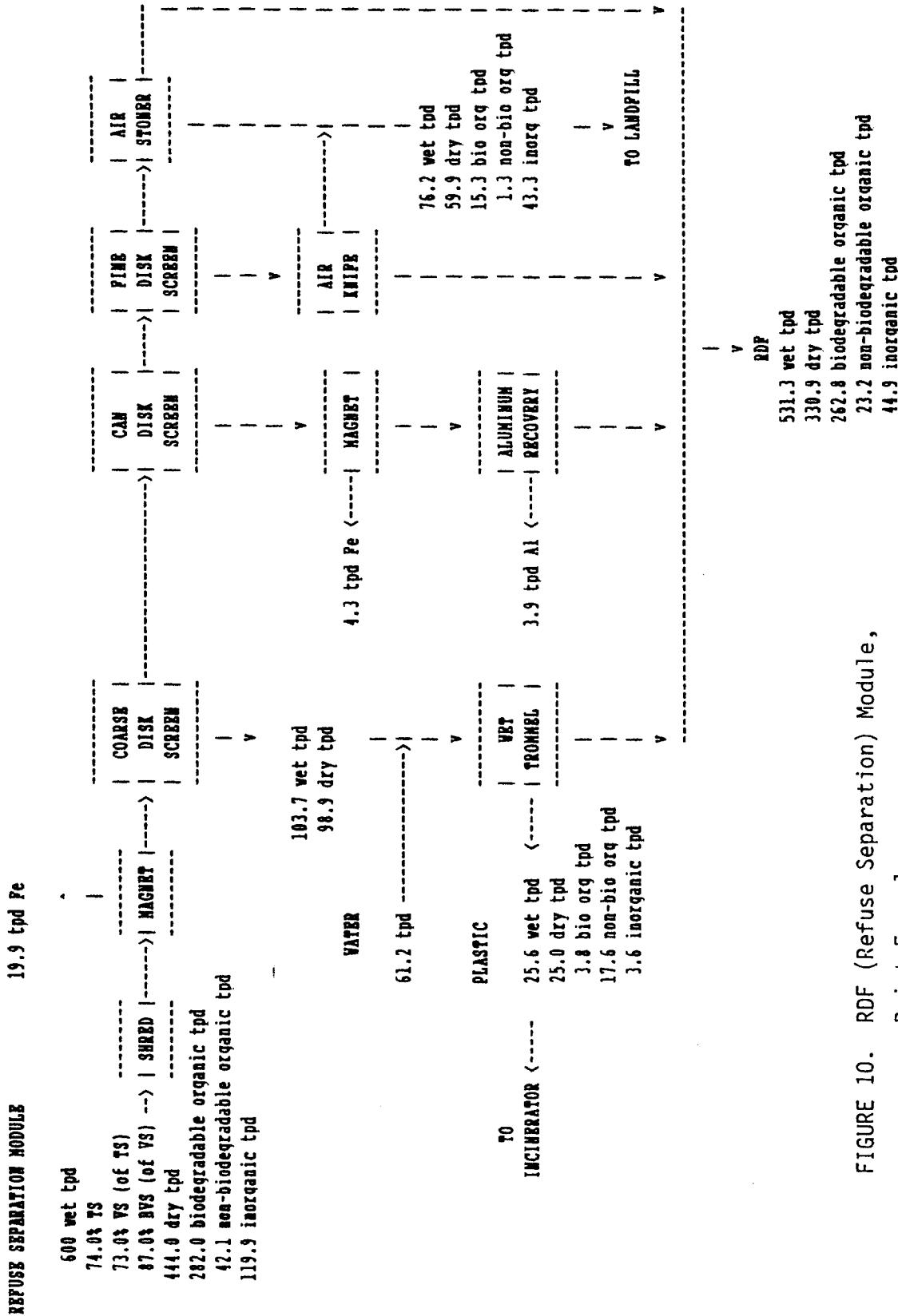


FIGURE 10. RDF (Refuse Separation) Module, Print Example

CONVERSION, HIGH MOISTURE FEEDS

0.06 10B12 Btu/year
 56.31 MMscf methane/year
 4.08 scf methane/lb VS_a
 280,485 scf biogas/day
 154,267 scf methane/day
 55 t methane
 10.3 dry tpd converted

0.3 tpd evaporated

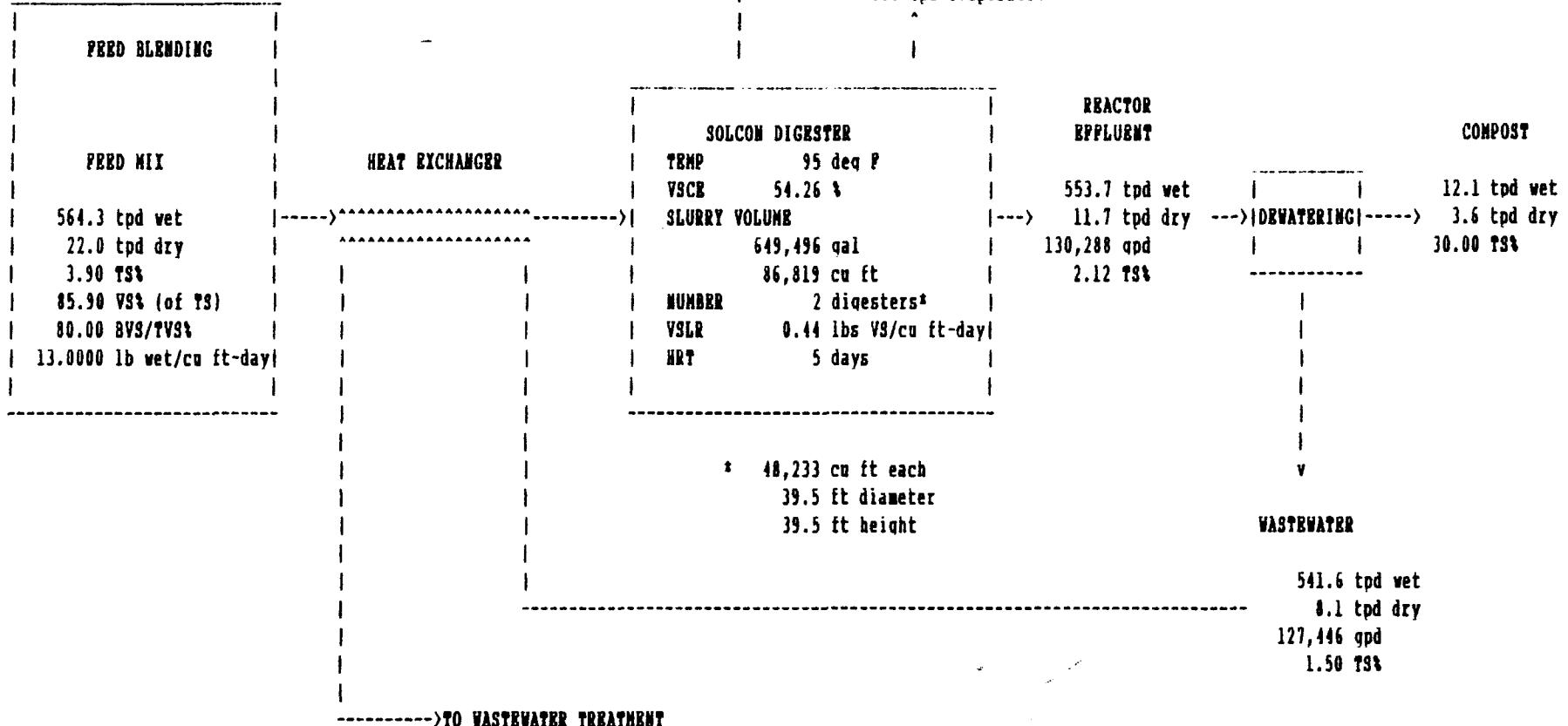


FIGURE 11. Conversion, High Moisture Feeds, Print Example

CONVERSION, LOW MOISTURE FEEDS

1.02 10E12 Btu/hr
 1017.33 MMScf methane/year
 4.87 scf methane/lb VFA
 5,067,638 scf biogas/day
 2,787,201 scf methane/day
 55 % methane
 198.7 dry tpd converted

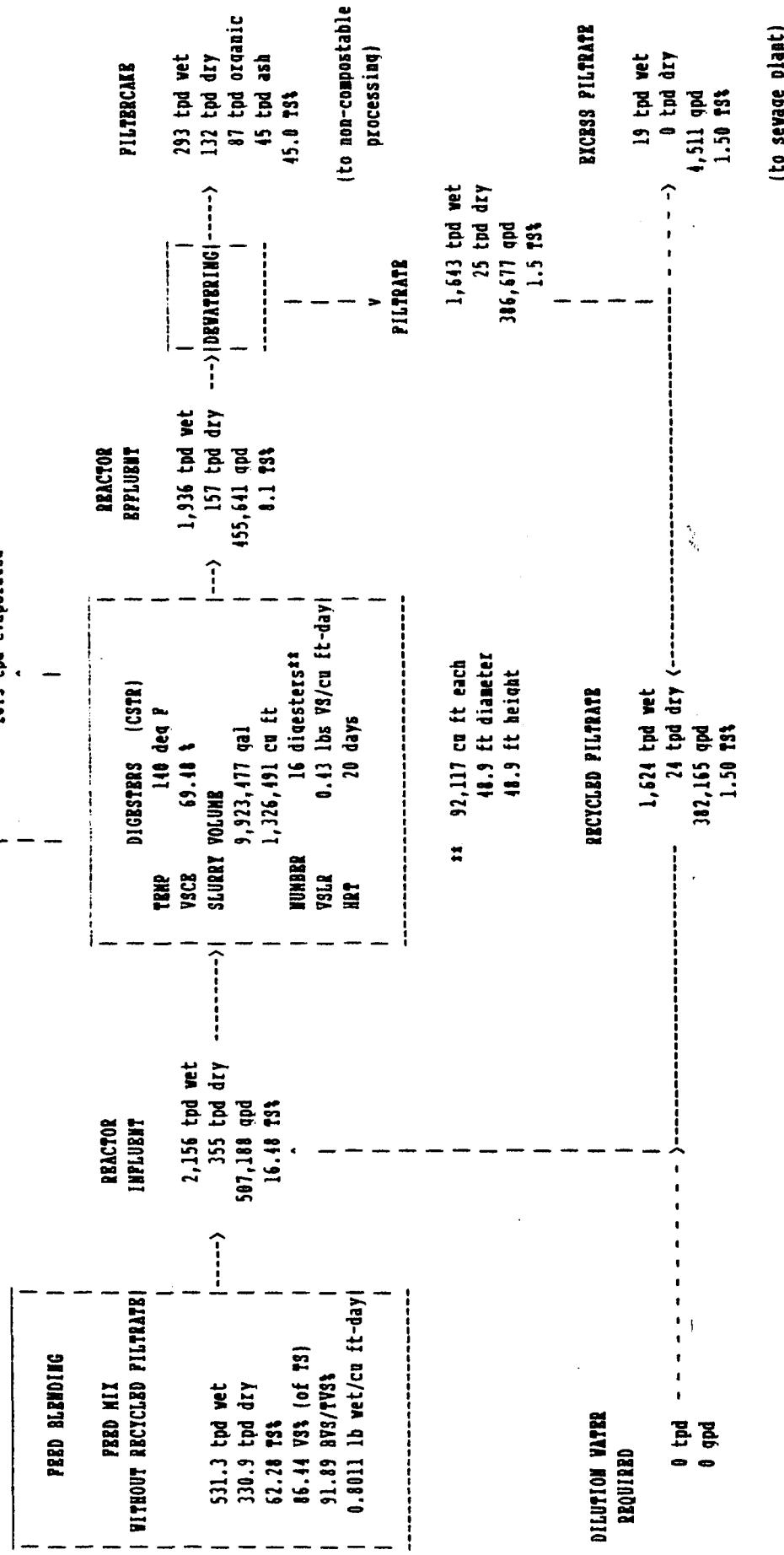
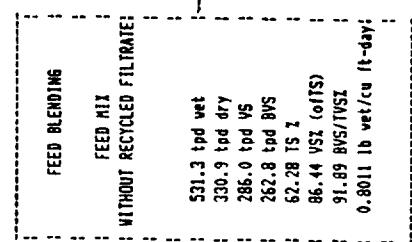


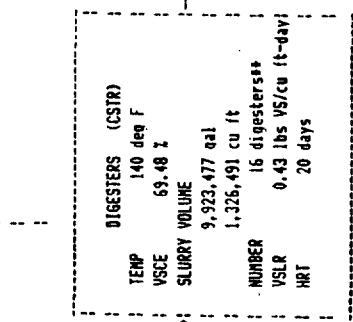
FIGURE 12. Conversion, Low Moisture Feeds, Print Example

CONVERSION, LOW MOISTURE FEEDS with WET OXIDATION OPTION

1.02 10E12 Btu/yr
1017.33 Mscf ethane/year
4.87 scf ethane/lb Vfa
5,067,638 scf biogas/day
2,787,201 scf ethane/day
55 L ethane
198.7 dry tpd converted



21.8 dry tpd converted



REACTOR
EFFLUENT

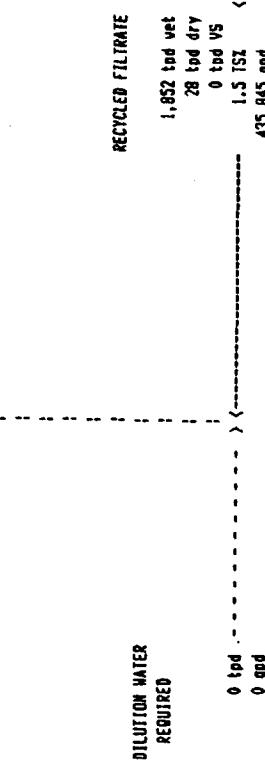
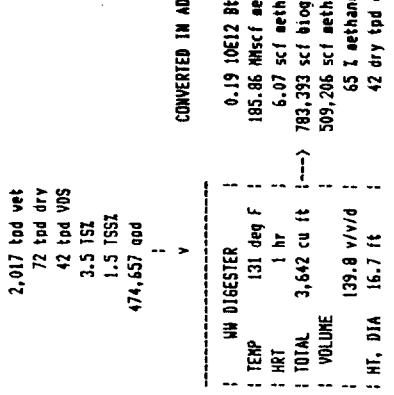
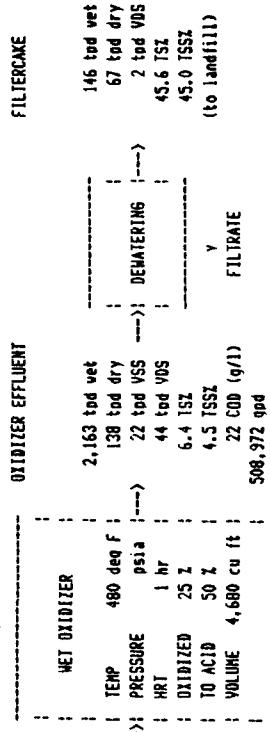


FIGURE 13. Conversion, Wet Oxidation, Print Example

GAS CLEANUP MODULE - PRISM MEMBRANE SYSTEM

BIOGAS PRODUCED		SYNTHETIC NATURAL GAS	
		95% METHANE CONTENT	
5.35 MMscf/day			2.79 MMscf/day
2,941 MMBtu/day-->	91% efficiency		2,647 MMBtu/day
55.00 t Methane	5,729 kWh per	(INCLUDING	90.00 t Methane
	MMscf biogas	RECYCLE)	recovery
	30,641 kWh/day		

ELECTRIC COMPRESSORS		PRISM SEPARATOR SYSTEM	
5.35 MMscf/day	1,162 kW		

V PERMEATE STREAM	
2.56 MMscf/day	
294 MMBtu/day	
11.40 t Methane in stream	

FIGURE 14. Gas Cleanup Module, Print Example

OPTION II - MEET PLANT HEAT REQUIREMENTS ONLY

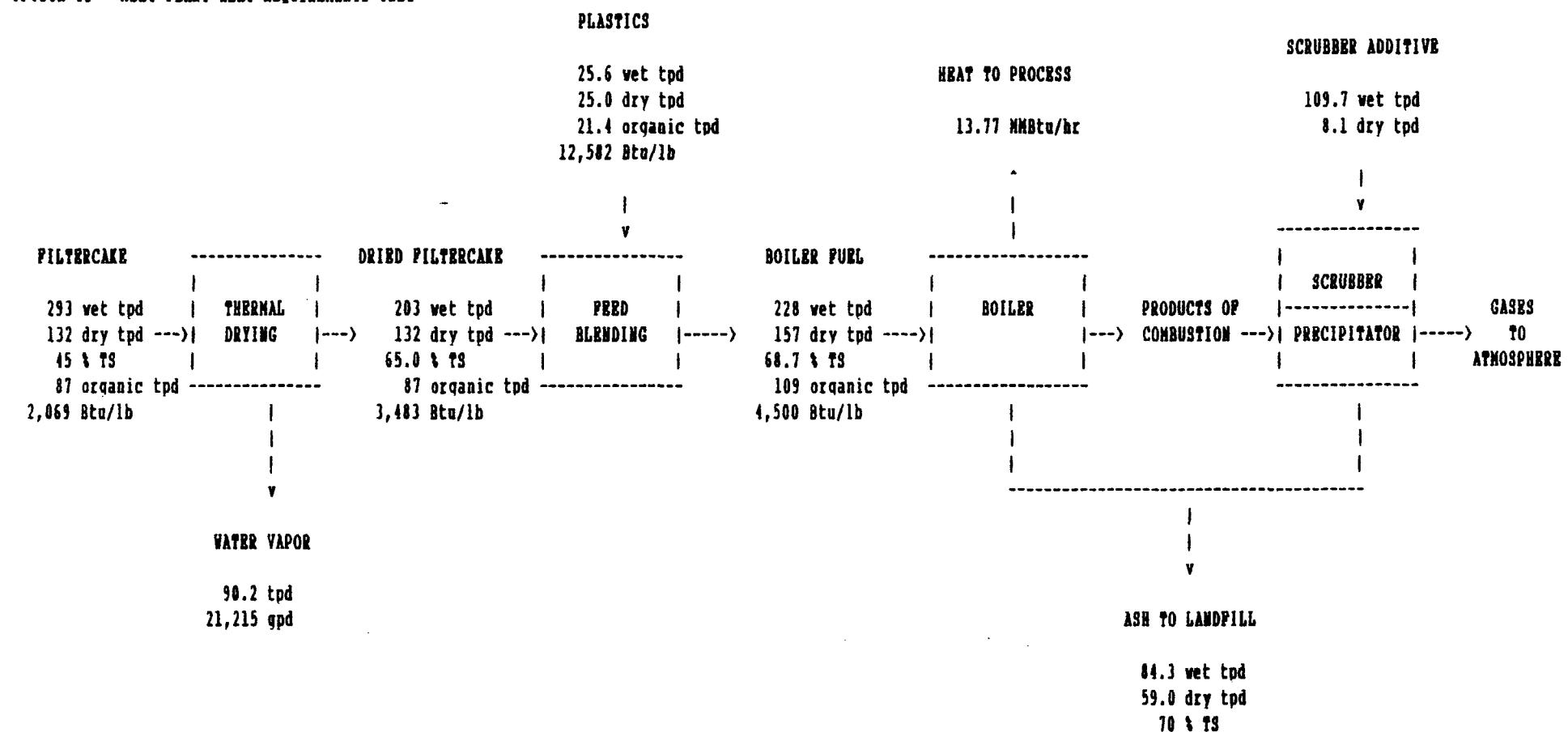


FIGURE 15. Residue Processing Thermal Only, Print Example

OPTION III - HEAT PLANT HEAT REQUIREMENTS & GENERATE ELECTRICITY

POWER TO PROCESS

93,799 kwh/day

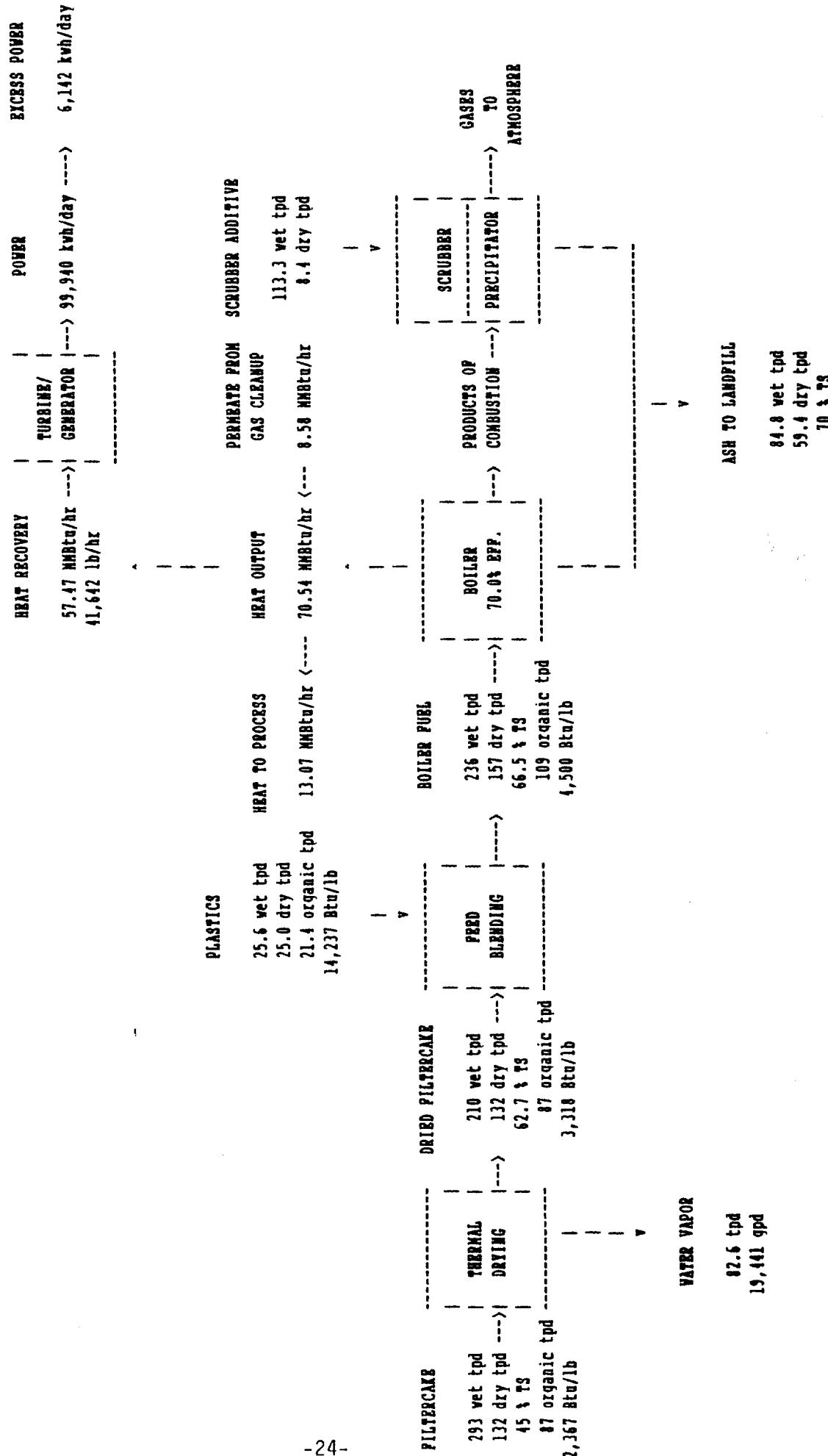


FIGURE 16. Residue Processing, Thermal & Power Print Example

LIST OF RANGE NAMES

<u>Range Name</u>	<u>Cell Address</u>	<u>Range Name</u>	<u>Cell Address</u>	<u>Range Name</u>	<u>Cell Address</u>
ADJ85	DM10	HARACRE	F177	PRAN5	CW1..DM253
ASSUMAC	B242	HIGHMO	AF1	PRIMINP	B207
ASSUMP	T1	IACRES	G119	PRINT	T196
AVTEMP	X15	IDAYS	G117	PRPMENU	T223
BIOMETH	AV164	IEFFBOD	G116	RDFBIO	L73
BLRBTU	AP171	IEFFTSS	G114	RDFDRY	L72
BLRIN	AP170	ILR	G118	RDFINORG	L75
CBMETH	AP6	INDEX1	B126	RDFNONBI	L74
CBSCF	AP4	INOUT	A5..R31	RDFWET	L71
CDIGTEMP	F24	INPUT	B202	REFBFLO	A48
CGCOUT	AG153	INTH	X17	REFDFLO	A47
CONTD1	U223	IOMENU	J227	REFIFLO	A50
CONVMENU	J235	IPDEPTH	G113	REFNFLO	A49
CORRECT1	H208	LEVCOIN	CW139	REFWFLO	A43
CORRECT2	H218	LEVOUT	CW224	RPMENU	J239
CORRECT3	H243	LOADING	I81	RSMOD	A41..R76
CORRECT4	P196	LOWMO	AF40	SEWTPD	G7
CORRECT5	P204	MACROS	A190	SEWTRMAC	B217
COSTMAC	J196	MAINMENU	B196	SRTRATD	G22
COSTMENU	J243	MAXDC	W8	SRTRATW	F22
COSTRANG	G18	MAXDD	Y8	STEP2	A105
COSTTAB	CW61..DD136	MAXHC	W7	STEP3	A140
CREDTAB	CW121	MAXHD	Y7	SUMMRY	A170..F178
DBMETH	AP45	MINNOC	W9	SWHMOD	A79
DBSCF	AP43	MINNOD	Y9	TECHOP	X10
DDIGTEMP	G24	MSWTPD	G8	TEPO	G13
DESTEMP	X16	MTMENU	J222	TRAVEL	J218
ELCOST	DA51	OPT2	BN25	TREACRE	F176
ELECREQ	AI244	OPT3	BN57	TSHY	B168
ENTER	J215	OUTPUT	I5..R31	TSSLU	B100
FEMENU	J231	PCONMENU	T215	UNITCOST	CW1
FIMOD	T27	PEMOD	AG187..AM244	VSSLU	B101
FINANMAC	J204	PERINCR	T189	WETOX	AF82..BL141
FLOMENU	T205	PONDIN	A113..G119	YEAR	G19
FLOW	G87	PONDOPT	A233	\O	B193
FUEL COST	DA52	PRAN1	A1..S248	\E	AN150
GCMOD	AV154	PRAN2	T1..AE248	\M	B194
GCOPT	X25	PRAN3	AF1..BL248	\X	B217
GROSPROD	AP175	PRAN4	BM1..CV248		